

# STACK EMISSIONS MONITORING REPORT



**SOCOTEC**

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#### Operator & Address:

Exxon Mobil  
Fife Ethylene Plant  
Mossmorran  
Cowdenbeath  
KY4 8EP

#### Permit Reference:

EPR Permit: PPC/A/1013494

#### Release Point:

A10 Boiler C

#### Sampling Date(s):

19 October 2021

SOCOTEC Job Number:	LEK 12957
Report Date:	17-Nov-21
Version:	1
Report By:	[Redacted]
MCERTS Number:	[Redacted]
MCERTS Level:	MCERTS Level 2 - Team Leader
Technical Endorsements:	1, 2, 3 & 4
Report Approved By:	[Redacted]
MCERTS Number:	[Redacted]
Business Title:	[Redacted]
Technical Endorsements:	1, 2, 3 & 4
Signature:	[Redacted]



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## EXECUTIVE SUMMARY

### MONITORING OBJECTIVES

Exxon Mobil operates a ethylene production process at Fife Ethylene Plant which is subject to EPR Permit PPC/A/1013494, under the Environmental Permitting Regulations 2010.

SOCOTEC LTD were commissioned by Exxon Mobil to carry out stack emissions monitoring to determine the release of prescribed pollutants from the following Plant under normal operating conditions.

The results of these tests shall be used to demonstrate compliance with a set of emission limit values for prescribed pollutants as specified in the Plant's EPR Permit, PPC/A/1013494.

#### **Plant**

A10 Boiler C

#### **Operator**

Exxon Mobil  
Fife Ethylene Plant  
Mossmorran  
Cowdenbeath  
KY4 8EP

EPR Permit: PPC/A/1013494

#### **Stack Emissions Monitoring Test House**

SOCOTEC - East Kilbride Laboratory  
2-4 Langlands Place  
Kelvin South Business Park  
East Kilbride  
G75 0YF  
UKAS and MCERTS Accreditation Number: 1015

Opinions and interpretations expressed herein are outside the scope of UKAS accreditation.  
The results of this testing relate only to the emission release point(s) listed in the report.  
MCERTS accredited results will only be claimed where both the sampling and analytical stages are MCERTS accredited.  
This test report shall not be reproduced, except in full, without written approval of SOCOTEC LTD.

## EXECUTIVE SUMMARY

EMISSIONS SUMMARY					
Parameter	Units	Result	Calculated Uncertainty +/-	Emission Limit Value (ELV)	Accreditation
Total Particulate Matter	mg/m <sup>3</sup>	1.04	0.42	5	MCERTS
Particulate Emission Rate	g/hr	54.0	21.9	-	
Sulphur dioxide	mg/m <sup>3</sup>	0.76	0.10	35	MCERTS
Sulphur dioxide Emission Rate	g/hr	39.5	5.26	-	
Oxides of Nitrogen (as NO <sub>2</sub> )	mg/m <sup>3</sup>	205	4.05	300	MCERTS
Oxides of Nitrogen (as NO <sub>2</sub> ) Emission Rate	g/hr	10652	211	-	
Carbon Monoxide	mg/m <sup>3</sup>	3.11	3.42	200	MCERTS
Carbon Monoxide Emission Rate	g/hr	162	178	-	
Oxygen	% v/v	4.02	0.09	6	MCERTS
Moisture	%	14.7	0.45	-	MCERTS
Stack Gas Temperature	°C	140	-	-	MCERTS
Stack Gas Velocity	m/s	13.5	0.33	-	
Gas Volumetric Flow Rate (Actual)	m <sup>3</sup> /hr	97429	5009	-	
Gas Volumetric Flow Rate (STP, Wet)	m <sup>3</sup> /hr	64667	3325	-	
Gas Volumetric Flow Rate (STP, Dry)	m <sup>3</sup> /hr	55140	2835	-	
Gas Volumetric Flow Rate at Reference Conditions	m <sup>3</sup> /hr	52077	2678	-	

ND = None Detected,

Results at or below the limit of detection are highlighted by bold italic text.

The above volumetric flow rate is an average of the data collected during the isokinetic tests. Mass emissions for non isokinetic tests are also calculated using these values.

Reference conditions are 273K, 101.3kPa, dry gas 3% Oxygen.

## EXECUTIVE SUMMARY

<b>MONITORING TIMES</b>			
<b>Parameter</b>	<b>Sampling Date(s)</b>	<b>Sampling Times</b>	<b>Sampling Duration</b>
Total Particulate Matter Run 1	19 October 2021	14:19 - 15:23	64 minutes
Sulphur dioxide Run 1	19 October 2021	14:19 - 15:23	64 minutes
Combustion Gases	19 October 2021	14:10 - 15:10	60 minutes
Preliminary Stack Traverse	19 October 2021	13:25	-

## EXECUTIVE SUMMARY

### PROCESS DETAILS

Parameter	Process Details
Description of process	Ethylene Production
Continuous or batch	Continuous
Product Details	Boiler generates process heat/steam
Part of batch to be monitored (if applicable)	Normal production
Normal load, throughput or continuous rating	85.27 % MCR
Fuel used during monitoring	3.24 t/h Fuel Gas
Abatement	None
Plume Appearance	None

## EXECUTIVE SUMMARY

### Monitoring Methods

The selection of standard reference / alternative methods employed by SOCOTEC is determined, wherever possible by the hierarchy of method selection outlined in Environment Agency technical Guidance 'Monitoring stack emissions: techniques and standards for periodic monitoring'.

MONITORING METHODS							
Species	Method Standard Reference Method / Alternative Method	SOCOTEC Technical Procedure	UKAS Lab Number	Method Accreditation	Limit of Detection (LOD)	Calculated MU +/- % Result	Calculated MU +/- % ELV
Total Particulate Matter	SRM - BS EN 13284-1	AE 104	1015	MCERTS	0.21 mg/m <sup>3</sup>	40.5%	8.44%
Sulphur dioxide	SRM - BS EN 14791	AE 112	1015	MCERTS	0.013 mg/m <sup>3</sup>	13.3%	0.29%
Oxides of Nitrogen	SRM - BS EN 14792:2017	AE 102	1015	MCERTS	0.54 mg/m <sup>3</sup>	2.0%	1.35%
Carbon Monoxide	SRM - BS EN 15058:2017	AE 102	1015	MCERTS	0.29 mg/m <sup>3</sup>	109.7%	1.6%
Oxygen	AM - BS EN 14789:2017	AE 102	1015	MCERTS	0.01%	2.3%	N/A - No ELV
Moisture	BS EN 14790	AE 105	1015	MCERTS	0.01%	3.0%	N/A - No ELV
Velocity	SRM - EN ISO 16911-1	AE 154	1015	MCERTS	5 Pa	2.4%	N/A - No ELV
Volumetric Flow Rate	SRM - EN ISO 16911-1	AE 154	1015	MCERTS	-	5.1%	N/A - No ELV

## EXECUTIVE SUMMARY

### Analytical Methods

The following tables list the analytical methods employed together with the custody details. Unless otherwise stated the samples are archived at the analysis lab location.

SAMPLING METHODS WITH SUBSEQUENT ANALYSIS							
Species	Analytical Technique	Analytical Procedure	UKAS Lab Number	Analysis Accreditation	Analysis Lab	Analysis Report number	Archive Period
Total Particulate Matter	Gravimetric	AE 106	1015	MCERTS	SOCOTEC (East Kilbride)	N/A	8 Weeks
Sulphur dioxide	Ion Chromatography	ASC/SOP/110	1252	MCERTS	SOCOTEC (Bretby)	ASC51261	8 Weeks

ON-SITE TESTING							
Species	Analytical Technique	Analytical Procedure	UKAS Lab Number	Accreditation	Laboratory	Data Archive Location	Archive Period
Oxides of Nitrogen	Chemiluminescence	AE 102	1015	MCERTS	SOCOTEC (East Kilbride)	SOCOTEC (East Kilbride)	5 years
Carbon Monoxide	Non Dispersive Infra Red	AE 102	1015	MCERTS	SOCOTEC (East Kilbride)	SOCOTEC (East Kilbride)	5 years
Oxygen	Zirconia Cell	AE 102	1015	MCERTS	SOCOTEC (East Kilbride)	SOCOTEC (East Kilbride)	5 years
Moisture	Gravimetric	AE 105	1015	MCERTS	SOCOTEC (East Kilbride)	-	-

## EXECUTIVE SUMMARY

SAMPLING LOCATION					
Sampling Plane Validation Criteria	Value	Units	Requirement	Compliant	Method
Lowest Differential Pressure	94	Pa	$\geq 5$ Pa	Yes	BS EN 15259
Lowest Gas Velocity	13.0	m/s	-	-	-
Highest Gas Velocity	13.9	m/s	-	-	-
Ratio of Gas Velocities	1.1	: 1	$< 3 : 1$	Yes	BS EN 15259
Mean Velocity	13.5	m/s	-	-	-
Maximum angle of flow with regard to duct axis	$< 15$	$^{\circ}$	$< 15^{\circ}$	Yes	BS EN 15259
No local negative flow	Yes	-	-	Yes	BS EN 15259

DUCT CHARACTERISTICS		
	Value	Units
Shape	Circular	-
Depth	1.60	m
Width	-	m
Area	2.01	m <sup>2</sup>
Port Depth	250	mm

SAMPLING LINES & POINTS		
	Isokinetic	Non-Iso & Gases
Sample port size	6" Flange	6" Flange
Number of lines used	1	1
Number of points / line	8	1
Duct orientation	Vertical	Vertical
Filtration	In Stack	In Stack
Filtration for TPM	In Stack	In Stack

SAMPLING PLATFORM	
General Platform Information	
Permanent / Temporary Platform / Ground level / Floor Level / Roof	Temporary
Inside / Outside	Outside

M1 Platform requirements	
Is there a sufficient working area so work can be performed in a compliant manner	No
Platform has 2 levels of handrails (approximately 0.5 m & 1.0 m high)	Yes
Platform has vertical base boards (approximately 0.25 m high)	Yes
Platform has removable chains / self closing gates at the top of ladders	Yes
Handrail / obstructions do not hamper insertion of sampling equipment	No
Depth of Platform = $>$ Stack depth / diameter + wall and port thickness + 1.5m	No

### Sampling Platform Improvement Recommendations (if applicable)

In order to comply with BS EN 15259 the platform should be extended/modified so that there is a minimum of 2.6m clearance from the sampling port to the edge of the platform on both sample lines.

## EXECUTIVE SUMMARY

### Sampling & Analytical Method Deviations

#### Sample Points

It is only possible to sample from one line therefore the number of sample points were doubled according to the MID BS EN 13284.

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APPENDIX 2 - Summaries, Calculations, Raw Data and Charts

APPENDIX 3 - Measurement Uncertainty Budget Calculations

APPENDIX 1 - Monitoring Schedule, Calibration Checklist & Monitoring Team

MONITORING SCHEDULE					
Species	Method Standard Reference Method / Alternative Method	SOCOTEC Technical Procedure	UKAS Lab Number	MCERTS Accredited Method	Number of Samples
Total Particulate Matter	SRM - BS EN 13284-1	AE 104	1015	MCERTS	1
Sulphur dioxide	SRM - BS EN 14791	AE 112	1015	MCERTS	1
Oxides of Nitrogen	SRM - BS EN 14792:2017	AE 102	1015	MCERTS	1
Carbon Monoxide	SRM - BS EN 15058:2017	AE 102	1015	MCERTS	1
Oxygen	AM - BS EN 14789:2017	AE 102	1015	MCERTS	1
Moisture	BS EN 14790	AE 105	1015	MCERTS	1
Velocity	SRM - EN ISO 16911-1	AE 154	1015	MCERTS	1

APPENDIX 1 - Monitoring Schedule, Calibration Checklist & Monitoring Team

CALIBRATEABLE EQUIPMENT CHECKLIST					
Extractive Sampling		Instrumental Analyser/s		Miscellaneous	
Equipment	Equipment I.D.	Equipment	Equipment I.D.	Equipment	Equipment I.D.
Control Box DGM	LEK 9.59	Horiba PG-250 Analyser	LEK 12.5	Laboratory Balance	LEK 15.21
Box Thermocouples	LEK 9.60	FT-IR Gasmet	-	Tape Measure	LEK 20.4
Meter In Thermocouple	LEK 9.60	FT-IR Oven Box	-	Stopwatch	-
Meter Out Thermocouple	LEK 9.60	Bernath 3006 FID	-	Protractor	-
Control Box Timer	LEK 17.33	Signal 3030 FID	-	Barometer	LEK 16.1
Oven Box	-	Servomex	-	Digital Micromanometer	LEK 1.2
Probe	LEK 6.44	JCT Heated Head Filter	-	Digital Temperature Meter	LEK 2.11
Probe Thermocouple	-	Thermo FID	-	Stack Thermocouple	LEK 3.117
Probe	-	Stackmaster	-	Mass Flow Controller	-
Probe Thermocouple	-	FTIR Heater Box for Heated Line	-	MFC Display module	-
S-Pitot	LEK 6.44	Anemometer	-	1m Heated Line (1)	-
L-Pitot	-	Ecophysics NOx Analyser	-	1m Heated Line (2)	-
Site Balance	LEK 23.20	Chiller (JCT/MAK 10)	LEK 12.16	1m Heated Line (3)	-
Last Impinger Arm	-	Heated Line Controller (1)	LEK 8.33	5m Heated Line (1)	LEK 8.33
Dioxins Cond. Thermocouple	-	Heated Line Controller (2)	LEK 8.51	10m Heated Line (1)	-
Callipers	LEK 15.1G	Site temperature Logger	-	10m Heated Line (2)	-
Small DGM	-			15m Heated Line (1)	-
Heater Controller	-			20m Heated Line (1)	LEK 8.51
Inclinometer (Swirl Device)	LEK 24.7			20m Heated Line (2)	-

NOTE: If the equipment I.D is represented by a dash (-), then this piece of equipment has not been used for this test.

CALIBRATION GASES					
Gas (traceable to ISO 17025)	Cylinder I.D Number	Supplier	ppm	%	Analytical Tolerance +/- %
Oxygen	194920	BOC	-	4.04	2.0
Nitric Oxide	LEK 165	BOC	198.8	-	2.0
Carbon Monoxide	LEK 260	BOC	162.6	-	2.0

**STACK EMISSIONS MONITORING TEAM**

MONITORING TEAM								
Personnel	MCERTS Number	MCERTS		TE / H&S Qualifications and Expiry Date				
		Level	Expiry	TE1	TE2	TE3	TE4	H&S
██████████	██████████	MCERTS Level 2	Apr-25	May-25	Nov-26	Dec-26	Mar-22	Apr-25
██████████	██████████	MCERTS Trainee	Mar-26	-	-	-	-	Mar-26

APPENDIX 2 - Summaries, Calculations, Raw Data and Charts

TOTAL PARTICULATE MATTER SUMMARY					
Parameter	Sampling Times	Concentration mg/m <sup>3</sup>	Uncertainty mg/m <sup>3</sup>	ELV mg/m <sup>3</sup>	Emission Rate g/hr
Run 1	14:19 - 15:23 19 October 2021	1.04	0.42	5	54.0
Blank	-	0.80	-	-	-

Reference conditions are 273K, 101.3kPa, dry gas 3% Oxygen.

Acetone Blank Value mg/l	Acceptable Value mg/l
0.3	10

**FILTER INFORMATION**

SAMPLES								
Test	Filter & Probe Rinse Number	Filter Start Weight g	Filter End Weight g	Mass Gained on Filter g	Probe Rinse Start Weight g	Probe Rinse End Weight g	Mass Gained on Probe g	Combined Total Mass Gained g
Run 1	AQ 4577	0.14550	0.14589	0.00039	201.96050	201.96120	0.00070	0.00109

If total mass gained is less than the LOD then the LOD is reported

BLANKS								
Test	Filter & Probe Number	Filter Start Weight g	Filter End Weight g	Mass Gained Filter g	Probe Start Weight g	Probe End Weight g	Mass Gained Probe g	Combined Total Mass Gained g
Run 1	AQ4432	0.15284	0.15373	0.00089	188.59990	188.59990	0.00000	0.00089

If total mass gained is less than the LOD then the LOD is reported

APPENDIX 2 - Summaries, Calculations, Raw Data and Charts

ISOKINETIC SAMPLING EQUATIONS - RUN 1			TPM		
<b>Absolute pressure of stack gas, P<sub>s</sub></b>			<b>Molecular weight of dry gas, M<sub>d</sub></b>		
Barometric pressure, P <sub>b</sub>	Kpa	101.8	CO <sub>2</sub>	%	0.00
Stack static pressure, P <sub>static</sub>	pa	-86.0	O <sub>2</sub>	%	4.02
P <sub>s</sub> = P <sub>b</sub> + P <sub>static</sub>	Kpa	101.7	Total	%	4.02
<b>Vol. of water vapour collected, V<sub>wstd</sub></b>			N <sub>2</sub> (100 -Total)	%	95.98
Moisture trap weight increase, Vlc	g	153.8	M <sub>d</sub> = 0.44(%CO <sub>2</sub> )+0.32(%O <sub>2</sub> )+0.28(%N <sub>2</sub> )		28.16
V <sub>wstd</sub> = (0.001246)(V <sub>lc</sub> )	m <sup>3</sup>	0.1916348	<b>Molecular weight of wet gas, M<sub>s</sub></b>		
<b>Volume of gas metered dry, V<sub>mstd</sub></b>			M <sub>s</sub> = M <sub>d</sub> (1 - B <sub>wo</sub> ) + 18(B <sub>wo</sub> )	g/gmol	26.66
Volume of gas sample through gas meter, V <sub>m</sub>		1.219	<b>Actual flow of stack gas, Q<sub>a</sub></b>		
Gas meter correction factor, Y <sub>d</sub>		0.976	Area of stack, A <sub>s</sub>	m <sup>2</sup>	2.01
Mean dry gas meter temperature, T <sub>m</sub>		296	Q <sub>a</sub> = (60)(A <sub>s</sub> )(V <sub>s</sub> )	m <sup>3</sup> /min	1611.2
Mean pressure drop across orifice, DH	mmH <sub>2</sub> O	42.379	<b>Total flow of stack gas, Q</b>		
V <sub>mstd</sub> = $\frac{(0.3592)(V_m)(P_b+(DH/13.6))(Y_d)}{T_m}$	m <sup>3</sup>	1.109	Conversion factor (K/mm.Hg)		0.3592
<b>Volume of gas metered wet, V<sub>mstw</sub></b>			Q <sub>std</sub> = $\frac{(Q_a)P_s(0.3592)(1-B_{wo})}{(T_s)}$	Dry	915.1
V <sub>mstw</sub> = V <sub>mstd</sub> + V <sub>wstd</sub>	m <sup>3</sup>	1.3008	Q <sub>stdO2</sub> = $\frac{(Q_a)P_s(0.3592)(1-B_{wo})(O_2REF)}{(T_s)}$	@O <sub>2</sub> ref	863.08
<b>Vol. of gas metered at O<sub>2</sub> Ref. Cond., V<sub>mstd@X%O2</sub></b>			Q <sub>stw</sub> = $\frac{(Q_a)P_s(0.3592)}{(T_s)}$	Wet	1073.23
Is the process burning hazardous waste? (If yes, no favourable oxygen correction)		No	<b>Percent isokinetic, %I</b>		
% oxygen measured in gas stream, act%O <sub>2</sub>		4.0	Nozzle diameter, D <sub>n</sub>	mm	7.03
% oxygen reference condition		3	Nozzle area, A <sub>n</sub>	mm <sup>2</sup>	38.86
O <sub>2</sub> Reference O <sub>2</sub> Ref = 21.0 - act%O <sub>2</sub>		0.94	Total sampling time, q	min	64
Factor $\frac{21.0 - ref\%O_2}{21.0 - act\%O_2}$			%I = $\frac{(4.6398E6)(T_s)(V_{mstd})}{(P_s)(V_s)(A_n)(q)(1-B_{wo})}$	%	98.0
V <sub>mstd@X%oxygen</sub> = (V <sub>mstd</sub> ) (O <sub>2</sub> Ref)	m <sup>3</sup>	1.0461	Acceptable isokinetic range 90% to 110%		Yes
<b>Moisture content, B<sub>wo</sub></b>			<b>Particulate Concentration, C</b>		
B <sub>wo</sub> = $\frac{V_{wstd}}{V_{mstd} + V_{wstd}}$	%	14.73	Mass collected on filter, M <sub>f</sub>	g	0.00039
<b>Moisture by FTIR</b>			Mass collected in probe, M <sub>p</sub>	g	0.00070
	%	-	Total mass collected, M <sub>n</sub>	g	0.00109
<b>Velocity of stack gas, V<sub>s</sub></b>			C <sub>wet</sub> = $\frac{M_n}{V_{mstw}}$	mg/m <sup>3</sup>	0.838
Velocity pressure coefficient, C <sub>p</sub>		0.84	C <sub>dry</sub> = $\frac{M_n}{V_{mstd}}$	mg/m <sup>3</sup>	0.983
Mean of velocity heads, DP <sub>avg</sub>	Pa	100.21	C <sub>dry@X%O2</sub> = $\frac{M_n}{V_{mstd@X\%oxygen}}$	mg/m <sup>3</sup>	1.042
Mean stack gas temperature, T <sub>s</sub>	K	411	<b>Particulate Emission Rates, E</b>		
Gas density (wet, ambient), p			E = $[(C_{wet})(Q_{stw})(60)] / 1000$		53.96
p = (M <sub>s</sub> *P <sub>s</sub> )/(8.314*T <sub>s</sub> )	kg/m <sup>3</sup>	0.793			
Stack Velocity, V <sub>s</sub>	$V_s = C_p \sqrt{\frac{\Delta DP_{avg}}{p}}$	m/s			
		13.35			

APPENDIX 2 - Summaries, Calculations, Raw Data and Charts

**TOTAL PARTICULATE MATTER QUALITY ASSURANCE CHECKLIST**

LEAK RATE						
Run	Mean Sampling Rate litre/min	Pre-sampling Leak Rate litre/min	Post-sampling Leak Rate litre/min	Maximum Vacuum mm Hg	Acceptable Leak Rate litre/min	Leak Tests Acceptable?
Run 1	18.60	0.20	-	-508	0.37	Yes

In BS EN 13284-1:2017 a post sampling leak check is not required.

ISOKINETICITY		
Run	Isokinetic Variation %	Acceptable Isokineticity
Run 1	98.00	Yes

Acceptable isokinetic range 90% to 110%

WEIGHING BALANCE UNCERTAINTY			
Run	Result mg/m <sup>3</sup>	5% ELV mg/m <sup>3</sup>	LOD < 5% ELV
Run 1	0.21	0.3	N/A - ELV <5 mg/m <sup>3</sup>

The above is based on both the Filter and rinse uncertainty  
Where installations have ELVs of 5 mg/m<sup>3</sup> or less, it may not be practical to meet the 5% of ELV requirement. Under these circumstances, a minimum one hour sample time shall used.

BLANK VALUE				
Run	Overall Blank Value mg/m <sup>3</sup>	Daily Emission mg/m <sup>3</sup>	Acceptable Blank Value mg/m <sup>3</sup>	Overall Blank Acceptable mg/m <sup>3</sup>
Blank 1	0.80	5	1.0	Yes

\*For ELVs of 5 mg/m<sup>3</sup> and lower a blank value must be <20% of the ELV

FILTERS					
Run	Filter Material	Filter Size mm	Max Filtration Temperature °C	Pre-use Filter Conditioning Temperature °C	Post-use Filter Conditioning Temperature °C
Run 1	Quartz Fibre	47	140	180	160

APPENDIX 2 - Summaries, Calculations, Raw Data and Charts

SULPHUR DIOXIDE SUMMARY					
Test	Sampling Times	Concentration mg/m <sup>3</sup>	LOD mg/m <sup>3</sup>	ELV mg/m <sup>3</sup>	Emission Rate g/hr
Run 1	14:19 - 15:23 19 October 2021	0.76	0.013	35	40
Field Blank	-	0.03	-	-	-

Reference conditions are 273K, 101.3kPa, dry gas 3% Oxygen.

**SULPHUR DIOXIDE QUALITY ASSURANCE CHECKLIST**

	Barometric Pressure  Kpa	Average Oxygen Value for %	Total Sample Volume @ ref Conditions m <sup>3</sup>	Mean Sampling Rate  l/min	Pre sampling leak rate  l/min	Post sampling leak rate  l/min	Acceptable leak rate  l/min	Leak Tests Acceptable?
Run 1	101.8	4.0	1.046	18.6	0.20	0.20	0.37	Yes

	Filter Material	Filter Size mm	Max. Filtration Temp. °C	Temperature during storage / transit <25°C	Type of Absorbers	Absorption Solutions
Run 1	Quartz Fibre	47	140	Yes	Glass	0.3% Hydrogen Peroxide

**SULPHUR DIOXIDE ABSORPTION EFFICIENCY**

Parameter	Total ug	IMP C ug	Absorption Efficiency %	Acceptable Absorption Efficiency %	Absorption Efficiency Acceptable ?
Run 1	798.7	13.3	98	95	Yes

ND - None Detected

APPENDIX 2 - Summaries, Calculations, Raw Data and Charts

ISOKINETIC SAMPLING EQUATIONS 1			Sulphur dioxide	
<b>Absolute pressure of stack gas, P<sub>s</sub></b>			<b>Velocity of stack gas, V<sub>s</sub></b>	
Barometric pressure, P <sub>b</sub>	kPa	102	Velocity pressure coefficient, C <sub>p</sub>	0.84
Stack static pressure, P <sub>static</sub>	Pa	-86	Mean of velocity heads, DP <sub>avg</sub>	Pa 100.21
P <sub>s</sub> = P <sub>b</sub> + (P <sub>static</sub> )	kPa	101.71	Mean stack gas temperature, T <sub>s</sub>	K 411.38
<b>Vol. of water vapour collected, V<sub>wstd</sub></b>			Gas density (wet, ambient), ρ	
Moisture trap weight increase, V <sub>lc</sub>	g	-	$\rho = (M_s * P_s) / (8.314 * T_s)$	kg/m <sup>3</sup> 0.793
V <sub>wstd</sub> = (0.001246)(V <sub>lc</sub> )	m <sup>3</sup>	-	Stack Velocity, V <sub>s</sub>	$V_s = C_p \sqrt{\frac{\Delta DP_{avg}}{\rho}}$ m/s 13.35
<b>Volume of gas metered dry, V<sub>mstd</sub></b>			<b>Actual flow of stack gas, Q<sub>a</sub></b>	
Volume of gas sample through gas meter, V <sub>m</sub>	m <sup>3</sup>	1.2190	Area of stack, A <sub>s</sub>	m <sup>2</sup> 2.01
Gas meter correction factor, Y <sub>d</sub>		0.9764	Q <sub>a</sub> = (60)(A <sub>s</sub> )(V <sub>s</sub> )	m <sup>3</sup> /min 1611
Mean dry gas meter temperature, T <sub>m</sub>	K	295.50	<b>Dry total flow of stack gas, Q<sub>std</sub></b>	
Mean pressure drop across orifice, DH	mmH <sub>2</sub> O	42.38	Conversion factor (K/mm.Hg)	0.3592
V <sub>mstd</sub> = $\frac{(0.3592)(V_m)(P_b + (DH/13.6))(Y_d)}{T_m}$	m <sup>3</sup>	1.11	Q <sub>std</sub> = $\frac{(Q_a)P_s(0.3592)(1-B_{wo})}{(T_s)}$	m <sup>3</sup> /min 915
<b>Volume of gas metered wet, V<sub>mstw</sub></b>			<b>Wet total flow of stack gas, Q<sub>stw</sub></b>	
V <sub>mstw</sub> = V <sub>mstd</sub> + V <sub>wstd</sub>	m <sup>3</sup>	1.3008	Q <sub>stw</sub> = $\frac{(Q_a)P_s(0.3592)}{(T_s)}$	m <sup>3</sup> /min 1073
<b>Vol. of gas metered at O<sub>2</sub> Ref. Cond., V<sub>mstd@X%O2</sub></b>			<b>Dry total flow of stack gas at X% O<sub>2</sub>, Q<sub>stdO2</sub></b>	
Is the process burning hazardous waste? (If yes, no favourable oxygen correction)	No		Q <sub>stdO2</sub> = $\frac{(Q_a)P_s(0.3592)(1-B_{wo})(O_2REF)}{(T_s)}$	m <sup>3</sup> /min 863
% oxygen measured in gas stream, act%O <sub>2</sub>	4.02		<b>Percent isokinetic, %I</b>	
% oxygen reference condition	3		Nozzle diameter, D <sub>n</sub>	mm 7.03
O <sub>2</sub> Reference $\frac{O_2 Ref = 21.0 - act\%O_2}{21.0 - ref\%O_2}$	0.94		Nozzle area, A <sub>n</sub>	mm <sup>2</sup> 38.86
Factor			Total sampling time, q	min 64
V <sub>mstd@X%oxygen</sub> = (V <sub>mstd</sub> )(O <sub>2</sub> Ref)	m <sup>3</sup>	1.0461	%I = $\frac{(4.6398E6)(T_s)(V_{mstd})}{(P_s)(V_s)(A_n)(q)(1-B_{wo})}$	% 98
<b>Moisture content, B<sub>wo</sub></b>			Acceptable isokinetic range 95% to 115%	
B <sub>wo</sub> = $\frac{V_{wstd}}{V_{mstd} + V_{wstd}}$	%	14.73	Yes	
<b>Moisture by FTIR</b>			<b>Sulphur dioxide Concentration, C</b>	
			Mass collected, M	
<b>Molecular weight of dry gas, M<sub>d</sub></b>			C <sub>wet</sub> = $\frac{M_n}{V_{mstw}}$ mg/m <sup>3</sup> 0.614	
CO <sub>2</sub>		0.00	C <sub>dry</sub> = $\frac{M_n}{V_{mstd}}$ mg/m <sup>3</sup> 0.720	
O <sub>2</sub>		4.02	C <sub>dry@X%O2</sub> = $\frac{M_n}{V_{mstd@X\%oxygen}}$ mg/m <sup>3</sup> 0.764	
Total		4.02		
N <sub>2</sub> (100 - Total)		95.98		
M <sub>d</sub> = 0.44(%CO <sub>2</sub> ) + 0.32(%O <sub>2</sub> ) + 0.28(%N <sub>2</sub> )		28.16	<b>Sulphur dioxide Emission Rates, E</b>	
<b>Molecular weight of wet gas, M<sub>s</sub></b>			E = $[(C_{wet})(Q_{stw})(60)] / 1000$ g/hr 39.54	
M <sub>s</sub> = M <sub>d</sub> (1 - B <sub>wo</sub> ) + 18(B <sub>wo</sub> )	g/gmol	26.7		

APPENDIX 2 - Summaries, Calculations, Raw Data and Charts

**COMBUSTION GASES SUMMARY**

Test	Sampling Time and Date	Concentration mg/m <sup>3</sup>	LOD mg/m <sup>3</sup>	ELV mg/m <sup>3</sup>	Emission Rate g/hr
Oxides of Nitrogen	14:10 - 15:10 19 October 2021	205	0.54	300	10652
Carbon Monoxide	14:10 - 15:10 19 October 2021	3.11	0.29	200	162.2

Test	Sampling Time and Date	Concentration %	LOD %
Oxygen	14:10 - 15:10 19 October 2021	4.02	0.01

Reference conditions are 273K, 101.3kPa, dry gas 3% Oxygen.

**PRE-SAMPLING CALIBRATION DATA**

Date	19 October 2021
Start Time	11:45
End Time	12:00

Chiller Temperature (°C)	2.8
Requirement	< 4°C
Compliant	Yes

Gas	Range (ppm / %)	Zero Reading at analyser	Span Reading at analyser	Zero Check at analyser	Zero Check down line	Span Check down line	Response Time (Secs)	Leak Rate %
Nitric Oxide	250	0.00	198.8	0.10	0.20	198.0	45	0.40
Carbon Monoxide	200	0.00	162.6	0.10	0.20	162.2	40	0.25
Oxygen	25	0.00	4.04	0.02	0.12	4.10	42	-1.49

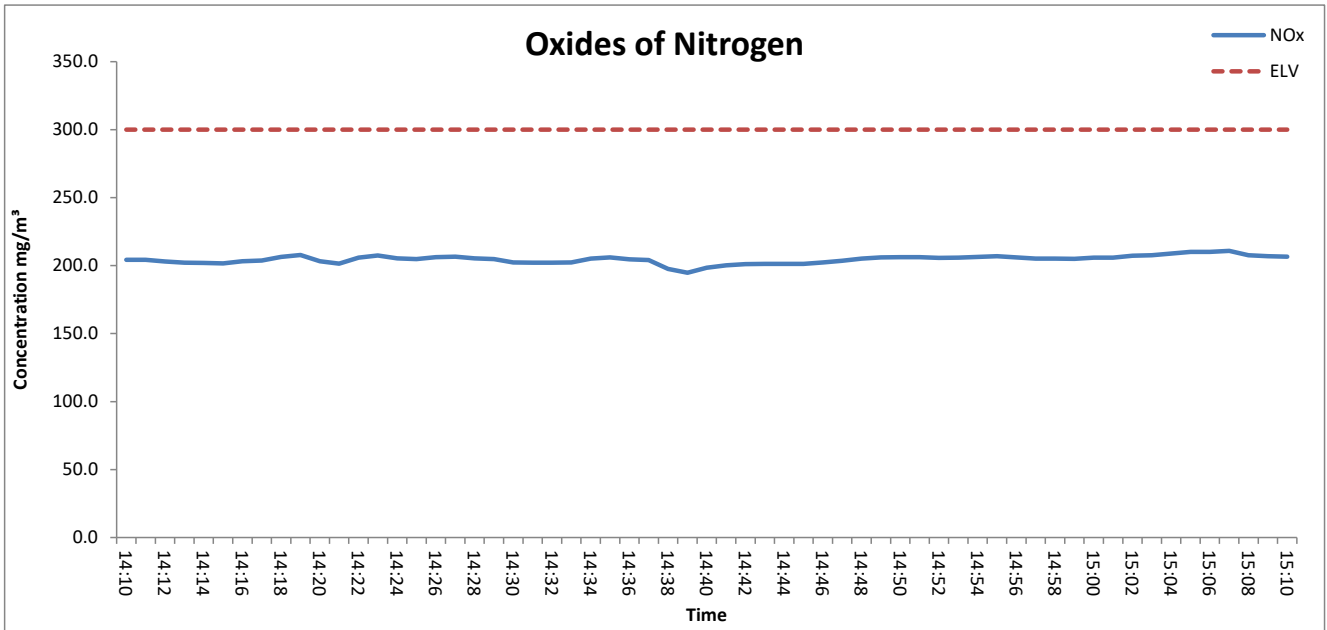
**POST-SAMPLING CALIBRATION DATA**

Date	19 October 2021
Start Time	15:15
End Time	15:30

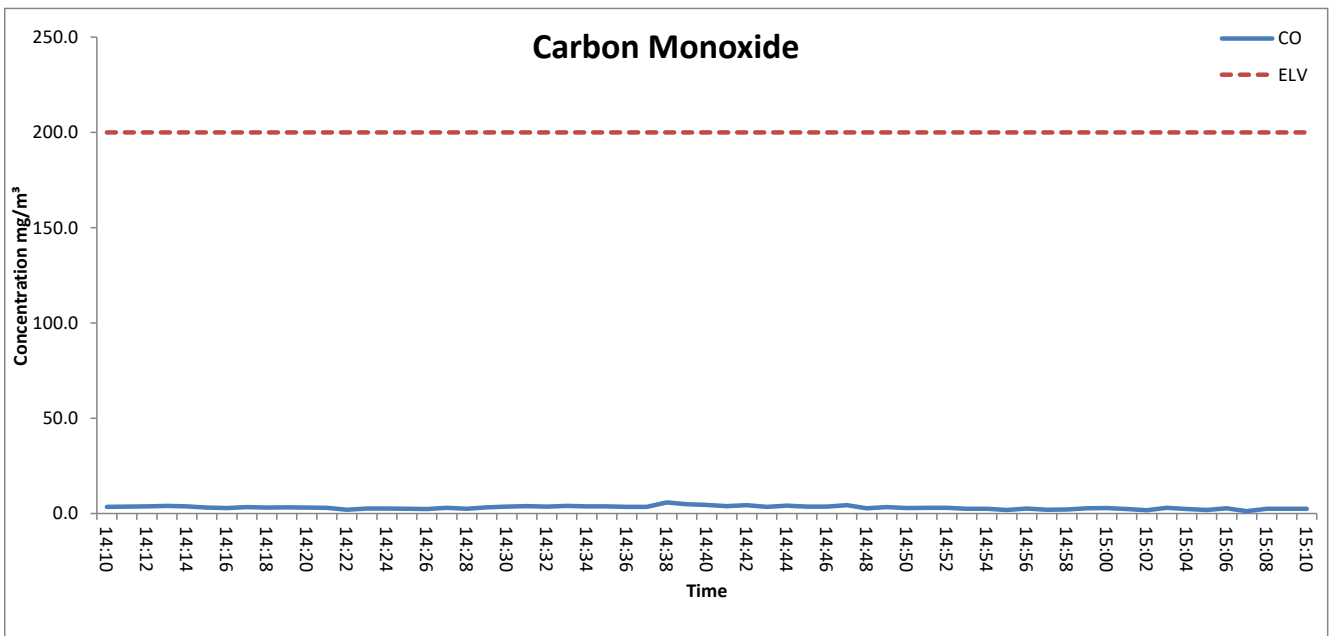
Chiller Temperature (°C)	2.4
Requirement	< 4°C
Compliant	Yes

Gas	Zero Check at Analyser	Span Check at Analyser	Zero Drift (%)	Span Drift (%)	Corrected for Zero Drift	Corrected for Span Drift	Corrected Values ppm / %
Nitric Oxide	0.20	197.5	0.05	-0.70	x	x	N/A - not corrected
Carbon Monoxide	-0.70	161.4	-0.49	-0.25	x	x	N/A - not corrected
Oxygen	0.10	4.12	1.99	0.00	x	x	N/A - not corrected

APPENDIX 2 - Summaries, Calculations, Raw Data and Charts  
**OXIDES OF NITROGEN (as NO<sub>2</sub>) EMISSIONS CHART**

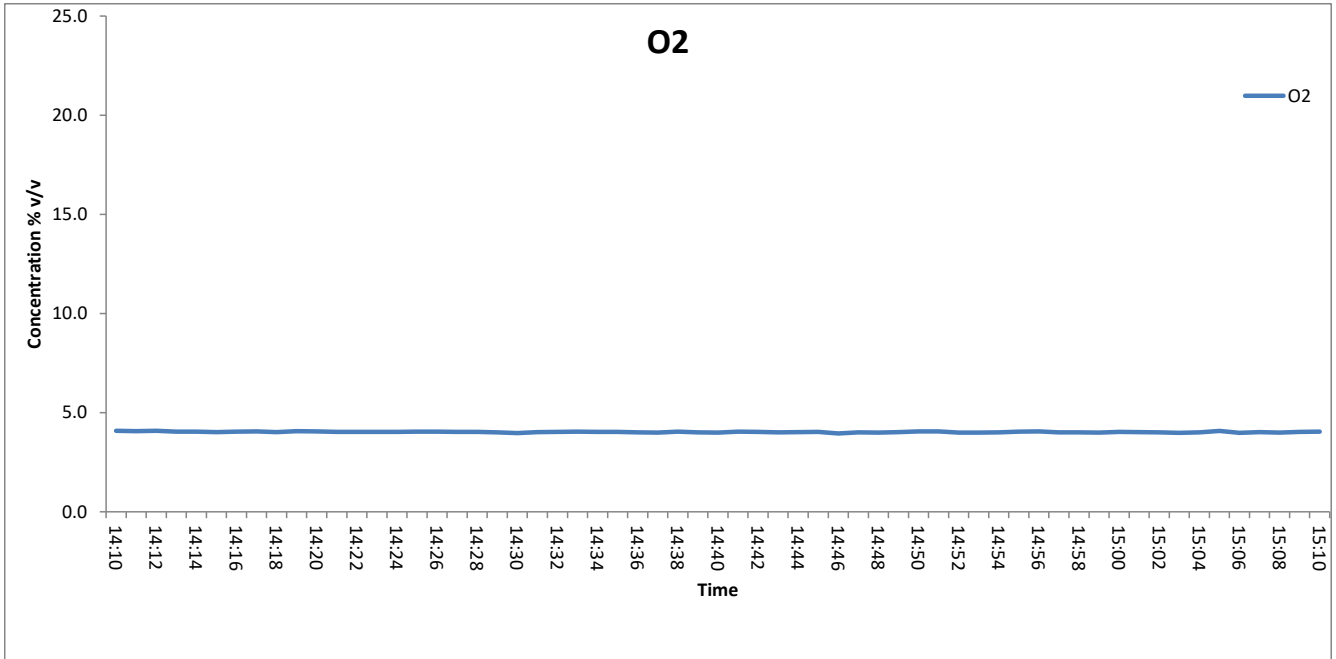


**CARBON MONOXIDE EMISSIONS CHART**



APPENDIX 2 - Summaries, Calculations, Raw Data and Charts

**OXYGEN EMISSIONS CHART**



APPENDIX 2 - Summaries, Calculations, Raw Data and Charts

**MOISTURE CALCULATIONS**

Moisture Determination - Isokinetic							
Test Number	Sampling Time and Date	Start Weight	End Weight	Total gain	Concentration	LOD	Uncertainty
		kg	kg	kg	%	%	%
Run 1	14:19 - 15:23 19 October 2021	3.4960	3.6498	0.1538	14.7	0.01	3.0

Moisture Quality Assurance							
Test Number	Sampling Duration	Total Volume Sampled	Sampling Rate	Start Leak Rate	End Leak Rate	Acceptable Leak Rate	Leak Tests Acceptable?
	mins	l	l/min	l/min	l/min	l/min	
Run 1	64	1301	18.6	0.20	-	0.37	Yes

**PRELIMINARY STACK SURVEY**

Stack Characteristics		
Stack Diameter / Depth, D	1.60	m
Stack Width, W	-	m
Stack Area, A	2.01	m <sup>2</sup>
Average stack gas temperature	140	°C
Stack static pressure	-0.084	kPa
Barometric Pressure	101.8	kPa

Stack Gas Composition & Molecular Weights								
Component	Molar Mass M	Density kg/m <sup>3</sup> p	Conc Dry % Vol	Dry Volume Fraction r	Dry Conc kg/m <sup>3</sup> pi	Conc Wet % Vol	Wet Volume Fraction r	Wet Conc kg/m <sup>3</sup> pi
CO <sub>2</sub>	44	1.963059	0.000000	0.000000	0.000000	0.000000	0.000000	0.000000
O <sub>2</sub>	32	1.427679	4.023607	0.040236	0.057444	3.430842	0.034308	0.048981
N <sub>2</sub>	28	1.249219	95.976393	0.959764	1.198956	81.836980	0.818370	1.022323
H <sub>2</sub> O	18	0.803070	-	-	-	14.732178	0.147322	0.118310

Where:  $p = M / 22.41$      $pi = r \times p$

Calculation of Stack Gas Densities		
Determinand	Result	Units
Dry Density (STP), $P_{STD}$	1.2564	kg/m <sup>3</sup>
Wet Density (STP), $P_{STW}$	1.1896	kg/m <sup>3</sup>
Dry Density (Actual), $P_{Actual}$	0.8339	kg/m <sup>3</sup>
Average Wet Density (Actual), $P_{ActualW}$	0.790	kg/m <sup>3</sup>

Where:

$P_{STD}$  = sum of component concentrations, kg/m<sup>3</sup> (not including water vapour)

$$P_{Actual} = P_{STD} \times (Ts / Ps) \times (Pa / Ta)$$

$P_{STW} = (P_{STD} + pi \text{ of H}_2\text{O}) / (1 + (pi \text{ of H}_2\text{O} / 0.8036))$

$$P_{ActualW} = P_{STW} \times (Ts / Ps) \times (Pa / Ta)$$

APPENDIX 2 - Summaries, Calculations, Raw Data and Charts

**PRELIMINARY STACK SURVEY**

**TRAVERSE 1**

Date of Survey	19 October 2021
Time of Survey	13:25
Velocity Measurement Device:	S-Type Pitot

Sampling Line A								
Traverse Point	Distance into duct (m)	DP pt Pa (average of 3 readings)	DP pt mmH <sub>2</sub> O (average of 3 readings)	Temp °C	Velocity m/s	Volumetric Flow Rate (actual) m <sup>3</sup> /s	O <sub>2</sub> % Vol	Angle of Swirl °
1	0.05	96.0	9.8	140	13.1	26.3	-	-
2	0.17	100.0	10.2	140	13.4	26.9	-	-
3	0.31	101.9	10.4	140	13.5	27.1	-	-
4	0.52	103.9	10.6	140	13.6	27.4	-	-
5	1.08	107.8	11.0	140	13.9	27.9	-	-
6	1.29	105.8	10.8	140	13.8	27.7	-	-
7	1.43	101.9	10.4	140	13.5	27.1	-	-
8	1.55	94.1	9.6	140	13.0	26.1	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
Mean	-	101.4	10.4	140	13.5	27.1	-	-

Sampling Line B								
Traverse Point	Distance into duct (m)	DP pt Pa (average of 3 readings)	DP pt mmH <sub>2</sub> O (average of 3 readings)	Temp °C	Velocity m/s	Volumetric Flow Rate (actual) m <sup>3</sup> /s	O <sub>2</sub> % Vol	Angle of Swirl °
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
Mean	-	-	-	-	-	-	-	-

**PRELIMINARY STACK SURVEY QUALITY ASSURANCE CHECKLIST**

PITOT LEAK CHECK								
Run	Pre Traverse Leak Rate				Post Traverse Leak Rate			
	Start Value mmH <sub>2</sub> O	End Value mmH <sub>2</sub> O	Difference %	Outcome	Start Value mmH <sub>2</sub> O	End Value mmH <sub>2</sub> O	Difference %	Outcome
Run 1	94	92	2.1	Pass	144	144	0.0	Pass

To complete a compliant pitot leak check a pressure of over 80 mmH<sub>2</sub>O (or 800 Pa) is applied and the pressure drop monitored over 5 mins. A drop of less than 5% must be observed.

S-Type Pitot Stagnation Check				
Run	Stagnation (Pa)	Reference (Pa)	Difference (Pa)	Outcome (Permitted +/- 10 Pa)
Run 1	-80	-88	8.0	Pass

APPENDIX 2 - Summaries, Calculations, Raw Data and Charts

**PRELIMINARY STACK SURVEY (CONTINUED)**

Sampling Plane Validation Criteria				
EA Technical Guidance Note (Monitoring) M1	Result	Units	Requirement	Compliant
Lowest Average Differential Pressure	94	Pa	>= 5 Pa	Yes
Lowest Gas Velocity	13.0	m/s	-	-
Highest Gas Velocity	13.9	m/s	-	-
Ratio of Gas Velocities	1.1	-	< 3 : 1	Yes
Maximum angle of flow with regard to duct axis	<15	°	< 15°	Yes
No local negative flow	Yes	-	-	Yes

Calculation of Stack Gas Velocity, V		
Velocity at Traverse Point, $V = K_{pt} \times (1-e) \times O(2 * DP_{pt} / P_{ActualW})$		
<b>Where:</b>		
$K_{pt}$ = Pitot tube calibration coefficient		
(1-e) = Compressibility correction factor, assumed at a constant 0.998		
Average Stack Gas Velocity, $V_a$	13.5	m/s

Calculation of Stack Gas Volumetric Flowrate, Q			
Duct gas flow conditions	Actual	Reference	Units
Temperature	140	0	°C
Total Pressure	101.716	101.3	kPa
Oxygen	4.0	3	%
Moisture	14.73	0.00	%
Pitot tube calibration coefficient, $K_{pt}$	0.84		

Gas Volumetric Flowrate	Result	Units
Average Stack Gas Velocity ( $V_a$ )	13.46	m/s
Stack Area (A)	2.01	m <sup>2</sup>
Gas Volumetric Flowrate (Actual), $Q_{Actual}$	97428.9	m <sup>3</sup> /hr
Gas Volumetric Flowrate (STP, Wet), $Q_{STP}$	64666.6	m <sup>3</sup> /hr
Gas Volumetric Flowrate (STP, Dry), $Q_{STP,Dry}$	55139.8	m <sup>3</sup> /hr
Gas Volumetric Flowrate (REF), $Q_{Ref}$	52076.5	m <sup>3</sup> /hr

**Where:**

$$Q_{Actual} = V_a \times A \times 3600$$

$$Q_{STP} = Q (Actual) \times (T_s / T_a) \times (P_a / P_s) \times 3600$$

$$Q_{STP,Dry} = Q (STP) / (100 - (100 / Ma)) \times 3600$$

$$Q_{Ref} = Q (STP) \times ((100 - Ma) / (100 - Ms)) \times ((21 - O_{2a}) / (21 - O_{2s}))$$

**Nomenclature:**

$T_s$  = Absolute Temperature, Standard Conditions, 273 K

$P_s$  = Absolute Pressure, Standard Conditions, 101.3 kPa

$T_a$  = Absolute Temperature, Actual Conditions, K

$P_a$  = Absolute Pressure, Actual Conditions, kPa

$Ma$  = Water vapour, Actual Conditions, % Vol

$Ms$  = Water vapour, Reference Conditions, % Vol

$O_{2a}$  = Oxygen, Actual Conditions, % Vol

$O_{2s}$  = Oxygen, Reference Conditions, % Vol



APPENDIX 3 - Measurement Uncertainty Budget Calculations

**MEASUREMENT UNCERTAINTY BUDGET - TOTAL PARTICULATE MATTER**

Run	Sampled Volume m <sup>3</sup>	Sampled Gas Temp K	Sampled Gas Pressure kPa	Sampled Gas Humidity % by volume	Oxygen Content % by volume	Limit of Detection % by mass	Leak %	Uncollected Mass mg
<b>MU required</b>	<b>≤ 2%</b>	<b>≤ 2%</b>	<b>≤ 1%</b>	<b>≤ 1%</b>	<b>≤ 10%</b>	<b>≤ 5% of ELV</b>	<b>≤ 2%</b>	<b>≤ 10% of ELV</b>
Run 1	0.002	2.0	0.50	1.0	0.1	0.2200	-	-
as a %	0.20	0.49	0.49	1.0	2.49	4.20617	1.08	0.018
<b>compliant?</b>	<b>Yes</b>	<b>Yes</b>	<b>Yes</b>	<b>Yes</b>	<b>Yes</b>	<b>Yes</b>	<b>Yes</b>	<b>Yes</b>

\*Where installations have ELVs of 5 mg/m<sup>3</sup> or less, it may not be practical to meet the 5% of ELV requirement. Under these circumstances, a minimum one hour sample time shall used.

Run	Volume (STP) m <sup>3</sup>	Mass of particulate mg	O <sub>2</sub> Correction -	Leak mg/m <sup>3</sup>	Uncollected Mass mg	Combined uncertainty
Run 1	0.74	1.0900	1.1	0.0065	0.0005	-
MU as mg/m <sup>3</sup>	0.01	0.2103	0.01	0.0065	0.0005	<b>0.21</b>
MU as %	1.25	20.1835	-	0.621	0.0471	-

<b>R1 - Uncertainty expressed at a 95% confidence level (where k = 2)</b>	<b>0.42</b>	<b>mg/m<sup>3</sup></b>	<b>40.48</b>	<b>% Result</b>	<b>8.44</b>	<b>% ELV</b>
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(k is a coverage factor which gives a 95% confidence in the quoted figures)

Reference – SOCOTEC Technical Procedure AE150 Estimation of Uncertainty of Measurement

APPENDIX 3 - Measurement Uncertainty Budget Calculations

**MEASUREMENT UNCERTAINTY BUDGET - ISOKINETIC SULPHUR DIOXIDE**

Run	Sampled Volume m <sup>3</sup>	Sampled Gas Temp K	Sampled Gas Pressure kPa	Sampled Gas Humidity % by volume	Oxygen Content % by volume	Limit of Detection % by mass	Leak %
<b>MU required</b>	<b>&lt;=2%</b>	<b>&lt;2.5 k</b>	<b>&lt;=1%</b>	<b>&lt;=1%</b>	<b>&lt;=5%</b>	<b>≤ 5% of ELV</b>	<b>&lt;=2%</b>
Run 1	1.046	296	100.94	1.0	4.024	1.1	-
as a %	0.10	0.68	0.50	1.0	2.49	0.09	1.08
<b>compliant?</b>	<b>Yes</b>	<b>Yes</b>	<b>Yes</b>	<b>Yes</b>	<b>Yes</b>	<b>Yes</b>	<b>Yes</b>

Run	Volume (STP) m <sup>3</sup>	Mass of Sulphur dioxide mg	O2 Correction -	Leak mg/m <sup>3</sup>	Lab Uncertainty mg	Combined uncertainty
Run 1	0.9630	1.1270	1.0603	0.0047	-	-
MU as mg/m <sup>3</sup>	0.0100	0.0332	0.0045	0.0047	0.0366	<b>0.0509</b>
MU as %	1.3093	4.3526	0.5891	0.6209	4.8	-

<b>R1 - Uncertainty expressed at a 95% confidence level (where k = 2)</b>	<b>0.10</b>	<b>mg/m<sup>3</sup></b>	<b>13.33</b>	<b>% Result</b>	<b>0.29</b>	<b>% ELV</b>
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(k is a coverage factor which gives a 95% confidence in the quoted figures)

Reference – SOCOTEC Technical Procedure AE150 Estimation of Uncertainty of Measurement



APPENDIX 3 - Measurement Uncertainty Budget Calculations

**MEASUREMENT UNCERTAINTY BUDGET - OXIDES OF NITROGEN**

Limit value	300	mg/m <sup>3</sup>
Concentration @ Ref conditions	204.5	mg/m <sup>3</sup>
Cal gas conc	408	mg/m <sup>3</sup>
Analyser Full Scale	513	mg/m <sup>3</sup>

	Value	Units	specification	MU Met?
Response time	45	seconds	180	Yes
Logger sampling interval	60	seconds	-	-
Measurement period	60	minutes	-	-
Number of readings in measurement	60	-	-	-
Repeatability at zero	0.11	% full scale	<1 % range	Yes
Repeatability at span level	0.1	% full scale	<2 % range	Yes
Deviation from linearity	-0.40	% of value	<2 % range	Yes
Zero drift	0.05	% full scale	<2% range / 24hr	Yes
Span drift	-0.70	% full scale	<2% range/24hr	Yes
volume or pressure flow dependence	0.25	% of full scale/3 kPa	<2 % / 3 kPa	Yes
atmospheric pressure dependence	0.25	% of full scale/2 kPa	<3% / 2 kPa	Yes
ambient temperature dependence zero / span	0.25	% full scale/10K	<3% range / 10 K	Yes
Combined interference	3.00	% range	<4% of Range	Yes
dependence on voltage	0.07	% full scale/10V	< 0.1%vol / 10 volt	Yes
Influence of Vibration	N/A	% of upper limit of Cal range	<2%	-
losses in the line (leak)	0.07	% of value	< 2% of value	Yes

Performance characteristic	Uncertainty	Value of uncertainty quantity
repeatability	$U_r = S_r$	0.0037
lack of fit	$U_{lof}$	-0.2309
short term zero drift	$U_{d,z}$	0.0295
short term span drift	$U_{d,s}$	-0.4066
influence of Ambient Temp at Zero	$U_{t,z}$	0.0072
influence of Ambient Temp at Span	$U_{t,s}$	0.1299
influence of sample gas pressure	$U_p$	0.0000
influence of sample gas flow	$U_{fit}$	0.1732
influence of supply voltage	$U_v$	0.2076
Combined Interference	$U_i$	0.0042
Uncertainty of Cal gas	$U_{adj}$	1.9880

Measurement uncertainty (Concentration Measured)	204.54	mg/m <sup>3</sup>
Combined uncertainty	2.06	mg/m <sup>3</sup>
Expanded at a 95% confidence interval	4.05	mg/m <sup>3</sup>

<b>Expanded uncertainty expressed with a level of confidence of 95%</b>	<b>1.35</b>	<b>% ELV</b>
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<b>Expanded uncertainty expressed with a level of confidence of 95%</b>	<b>4.0</b>	<b>mg/m<sup>3</sup></b>
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<b>Expanded uncertainty expressed with a level of confidence of 95%</b>	<b>2.0</b>	<b>% value</b>
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Developed for the STA by [redacted] NPL

APPENDIX 3 - Measurement Uncertainty Budget Calculations

**MEASUREMENT UNCERTAINTY BUDGET - CARBON MONOXIDE**

Limit value	200	mg/m <sup>3</sup>
Concentration @ Ref conditions	3.1	mg/m <sup>3</sup>
Cal gas conc	203.3	mg/m <sup>3</sup>
Analyser Full Scale	250	mg/m <sup>3</sup>

Performance characteristics	Value	Units	specification	MU Met?
Response time	40	seconds	180	Yes
Logger sampling interval	60	seconds	-	-
Measurement period	60	minutes	-	-
Number of readings in measurement	60	-	-	-
Repeatability at zero	0.1	% full scale	<1 % range	Yes
Repeatability at span level	0.2	% full scale	<2 % range	Yes
Deviation from linearity	0.61	% of value	<2 % range	Yes
Zero drift	-0.49	% full scale	<2% range / 24hr	Yes
Span drift	-0.25	% full scale	<2% range/24hr	Yes
volume or pressure flow dependence	0.2	% of full scale/3 kPa	<2 % / 3 kPa	Yes
atmospheric pressure dependence	0.44	% of full scale/2 kPa	<3% / 2 kPa	Yes
ambient temperature dependence zero / span	1	% full scale/10K	<3% range / 10 K	Yes
Combined interference	0.03	% of Range	<4% of Range	Yes
dependence on voltage	-0.06	% full scale/10V	< 0.1%vol /10 volt	Yes
Influence of Vibration	N/A	% of upper limit of Cal range	<2%	N/A
losses in the line (leak)	0.00	% of value	< 2% of value	Yes
Uncertainty of calibration gas	1.00	% of value	< 2% of value	Yes

N/A - Horiba's are not effected by Vibration

Performance characteristic	Uncertainty	Value of uncertainty quantity
repeatability	$U_r = S_r$	0.003
lack of fit	$U_{lof}$	0.12
short term zero drift	$U_{d,z}$	0.35
short term span drift	$U_{d,s}$	-0.28
influence of Ambient Temp zero	$U_{t,z}$	-0.02
influence of Ambient Temp span	$U_{t,s}$	0.01
influence of sample gas pressure	$U_p$	0.00
influence of sample gas flow	$U_{fit}$	0.14
influence of supply voltage	$U_v$	-0.09
Combined Interference	$U_i$	1.34
Uncertainty of Cal gas	$U_{adj}$	0.81

Measurement uncertainty (Concentration Measured)	2.9	mg/m <sup>3</sup>
Combined uncertainty	1.6	mg/m <sup>3</sup>
Expanded uncertainty	3.2	mg/m <sup>3</sup>

<b>Expanded uncertainty expressed with a level of confidence of 95%</b>	<b>1.6</b>	<b>% ELV</b>
<b>Expanded uncertainty expressed with a level of confidence of 95%</b>	<b>3.2</b>	<b>mg/m<sup>3</sup></b>
<b>Expanded uncertainty expressed with a level of confidence of 95%</b>	<b>109.7</b>	<b>% value</b>

Developed for the STA by [redacted] NPL

Reference – SOCOTEC Technical Procedure AE150 Estimation of Uncertainty of Measurement

APPENDIX 3 - Measurement Uncertainty Budget Calculations

**MEASUREMENT UNCERTAINTY BUDGET - OXYGEN**

Reference	3	%vol
Reported Concentration	4.02	%vol
Calibration gas	4.04	%vol
Analyser Full Scale	25	%vol

	Value	Units	specification	MU Met?
Response time	42	seconds	180	Yes
Logger sampling interval	60	seconds	-	-
Measurement period	60	minutes	-	-
Number of readings in measurement	60	-	-	-
Repeatability at zero	0.25	% full scale	<1 % range	Yes
Repeatability at span level	0.15	% full scale	<2 % range	Yes
Deviation from linearity	0.13	% of value	<2 % range	Yes
Zero drift	1.99	% full scale	<2% range / 24hr	Yes
Span drift	0.00	% full scale	<2% range/24hr	Yes
volume or pressure flow dependence	0.03	% of full scale/3 kPa	<2 % / 3 kPa	Yes
atmospheric pressure dependence	0.05	% of full scale/2 kPa	<3% / 2 kPa	Yes
ambient temperature dependence	-0.08	% full scale/10K	<3% range / 10 K	Yes
Combined interference	0.14	% range	<4% of Range	Yes
dependence on voltage	0.00	% full scale/10V	< 0.1%vol /10 volt	Yes
losses in the line (leak)	0.14	% of value	< 2% of value	Yes
Uncertainty of calibration gas	0.1	% of value	< 2% of value	Yes

Performance characteristic	Uncertainty	Value of uncertainty quantity
repeatability	$U_r = S_r$	0.0083
lack of fit	$U_{lof}$	0.0751
short term zero drift	$U_{dz}$	1.1490
short term span drift	$U_{ds}$	0.0000
influence of Ambient Temp at Zero	$U_{tz}$	0.0000
influence of Ambient Temp at Span	$U_{ts}$	-0.0003
influence of sample gas pressure	$U_p$	0.0000
influence of sample gas flow	$U_{fit}$	0.0173
influence of supply voltage	$U_v$	0.0001
Combined Interference	$U_i$	0.0485
Uncertainty of Cal gas	$U_{adj}$	0.0202

Measurement uncertainty (Concentration Measured)	4.02	%
Combined uncertainty	1.15	%
Expanded uncertainty	2.26	%

Expanded uncertainty expressed with a level of confidence of 95%	2.3	%
Expanded uncertainty expressed with a level of confidence of 95%	56.15	% vol

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APPENDIX 3 - Measurement Uncertainty Budget Calculations

**MEASUREMENT UNCERTAINTY BUDGET - VELOCITY & VOLUMETRIC FLOW RATE**

Measured Velocity at Actual Conditions	13.5	m/s
Measured Volumetric Flow rate at Actual Conditions	97429	m <sup>3</sup> /hr

Performance Characteristics & Source of Value	Units	Values	Requirement	Compliant
Uncertainty of Local Gas Velocity Determination	-	0.010		
Uncertainty of pitot tube coefficient	-	0.90		
Uncertainty of mean local dynamic pressures	-	0.591	minimum 3	Yes
Factor loading, function of the number of measurements.	3 readings			
Range of measurement device	pa	1000		
Resolution	pa	1.00		
Calibration uncertainty	pa	16.57	<1% of Value or 20 Pa whichever is greater	Yes
Drift	% range	0.10		
Linearity	% range	0.06	<2% of value	Yes
Uncertainty of gas density determination				
Uncertainty of molar mass determination	kg/mol	0.00005		
Uncertainty of temperature measurement	K	2.11	<1% of value	Yes
Uncertainty of absolute pressure in the duct	pa	519		
Uncertainty associated with the estimate of density	-	0.008		
Uncertainty associated with the measurement of local velocity	-	0.0001		
Uncertainty associated with the measurement of mean velocity	-	0.0002		

Measurement Uncertainty - Velocity	m/s
Combined uncertainty	0.17
Expanded uncertainty at a 95% Confidence Interval	0.33

Note - The expanded uncertainty uses a coverage factor of  $k = 2$ .

Expanded Measurement Uncertainty of Velocity at a 95% Confidence Interval	%
Expressed as a % of the Measured Velocity	1.2
Expanded uncertainty at a 95% Confidence Interval	2.4

Measurement Uncertainty Volumetric Flow Rate	m <sup>3</sup> /hr
Combined uncertainty	2556
Expanded uncertainty at a 95% Confidence Interval	5009

Note - The expanded uncertainty uses a coverage factor of  $k = 2$ .

Expanded Measurement Uncertainty of Volumetric Flow Rate at a 95% Confidence Interval	%
Expressed as a % of the Measured Volumetric Flow Rate	2.6
Expanded uncertainty at a 95% Confidence Interval	5.1

Reference – SOCOTEC Technical Procedure AE150 Estimation of Uncertainty of Measurement

## END OF REPORT

*Thank you for choosing SOCOTEC for your environmental monitoring needs. We hope our services have met your requirements and that you are fully satisfied with your experience of working with us, we really do value your custom and would welcome your feedback. We would appreciate it if you could take a moment to complete a short online questionnaire so that we can improve our operations and address any areas that have not met with your expectations, by clicking on the following*

[https://www.surveymonkey.co.uk/r/CAE\\_customer\\_feedback\\_weblink](https://www.surveymonkey.co.uk/r/CAE_customer_feedback_weblink)